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The pseudoparticulate expansion of screen-packed gas-fluidized beds, Capes, C. E., and A. E. McIlhinney, **AIChE Journal, 14,** No. 6, p. 917 (November, 1968).

Key Words: A. Expansion-8, Fluidized Beds-9, Lead-9, Nickel-9, Sand-9, Glass-9, Air-5, Carbon Dioxide-5, Helium-5, Columns-10, Packing-10, 6. Screens-10, Bubbles-9, Size-7, Porosity-7, Density-7.

Abstract: A study was made of the expansion characteristics of beds of uniformly-sized spherical particles of lead, nickel, sand, glass, and plastic fluidized with air, carbon dioxide, and helium in columns packed with open-ended cylindrical screen packing. The addition of packing to a gas-fluidized bed limits the bubble size, prevents slugging and allows beds of high aspect ratio to expand smoothly in a manner similar to the behavior of liquid-fluidized beds.

Calorimetric determination of the isothermal effect of pressure on the enthalpy of methane and two methane-propane mixtures, Dillard, D. D., W. C. Edmister, J. H. Erbar, and R. L. Robinson, Jr., **AIChE Journal, 14,** No. 6, p. 923 (November, 1968).

Key Words: A. Pressure-6, Enthalpy-7, 8, 9, Isothermal-0, Methane-9, Propane-9, Mixtures-9, Calorimeter-10, Vapor Phase-0, Comparisons-8, Calculation-9, Experiments-9, Alkanes-9, Benedict-Webb-Rubin Equation-10, Redlich-Kwong Equation-10, Equations of State-10, Aliphatic Compounds-9, Hydrocarbons-9.

Abstract: Isothermal effects of pressure on the enthalpy of methane and two methane-propane mixtures were measured in the vapor region. Comparisons of measured values were made with enthalpy values calculated by equations of state.

Condensation from superheated gas-vapor mixtures, Stern, Frederick, and Ferdinand Votta, Jr., **AIChE Journal, 14,** No. 6, p. 928 (November, 1968).

Key Words: A. Condensation-8, Heat Transfer-8, Mass Transfer-8, Mixtures-9, Superheated-0, Water-9, Air-9, Carbon Dioxide-9, Helium-9, Dehumidification-8, Theoretical-0, Experimental-0, Digital Computer-10.

Abstract: Superheated mixtures of vapor and noncondensable gas were cooled and condensed in downflow inside a single tube vertical condenser. The systems studied were air-water, carbon dioxide-water and helium-water. A theoretical solution of the problem was solved rigorously on a digital computer. Results indicated excellent agreement between the theoretical and experimental cooling paths and the required transfer area.

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ERRATA

In the paper "Stability of Adiabatic Packed Bed Reactors: Effect of flow variations and coupling between the particles," by John W. Vanderveen, Dan Luss, and Neal R. Amundson [Vol. 14, p. 636 (1968)], Equations (36), (37), and (38) should read as follows:

$$\frac{1}{\beta p_{pj}} > \frac{H+1}{H}\left(\frac{M}{M+\delta_j}\right)\frac{d\,\delta_j}{dt_{pj}}(1+k_j) \quad (36)$$

$$\frac{dQ_I}{dt_{pj}} > (1+k_j)\frac{(H+1)}{H}\left(\frac{M}{M+\delta_j}\right)\frac{dQ_{II}}{dt_{pj}} \quad (37)$$

$$(1+k_j)\frac{H+1}{H}\left(\frac{M}{M+\delta_j}\right) > 1 \quad (38)$$

Neal R. Amundson

In the paper "A Computational Model for the Structure of Porous Materials Employed in Catalysis" by R. N. Foster and J. B. Butt [Vol. 12, p. 180 (1966)], the following sentence should be added immediately following Equation (11):

In practice, however, this normalization yields very large values of i for the microporous structure and very small values for the macroporous structure: this problem is avoided by weighting the distribution according to the logarithmic ratio of pore lengths.

The aid of Henry Hanes in pointing out the omisson is acknowledged.

J. B. Butt

In "Behavior of Non-Newtonian Fluids in the Inlet Region of a Channel" by Morton Collins and W. R. Schowalter [Vol. 9, No. 1, p. 98 (1963)], the second term on the right-hand side of Equation (28) should contain the factor $n^n/(2n + 1)^{n-1}$. This factor, though missing in the text, was included in all of the calculations based upon Equation (28).

W. R. Schowalter